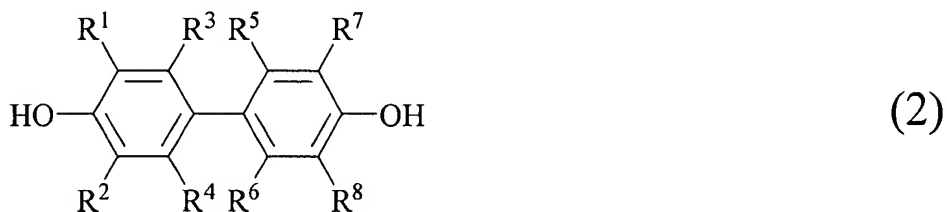
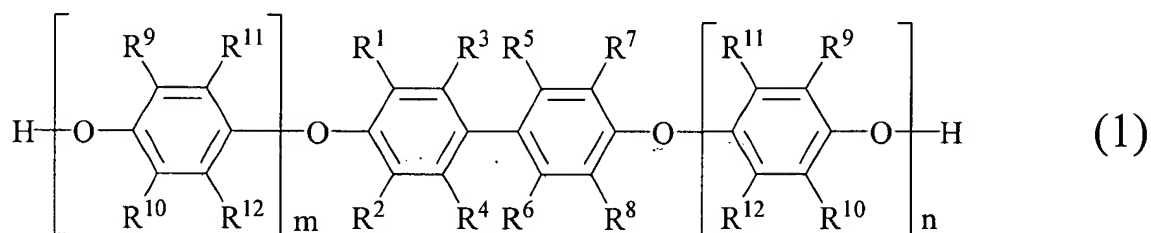


AMENDMENTS TO THE CLAIMS

1. (Currently Amended) A process for the production of a bifunctional phenylene ether oligomer compound having no amine adduct represented by the formula (1), which process comprises oxidatively polymerizing a bivalent phenol of the formula (2) and a monovalent phenol of the formula (3) in the presence of a copper-containing catalyst and a mixture consisting of a secondary amine having a secondary alkyl group, a tertiary alkyl group or an aryl group with a tertiary amine

[Chemical formula 1]



wherein $\text{R}^1, \text{R}^2, \text{R}^3, \text{R}^7, \text{R}^8, \text{R}^9$ and R^{10} are the same or different and represent a halogen atom, an alkyl group having 6 or less carbon atoms or a phenyl group, $\text{R}^4, \text{R}^5, \text{R}^6, \text{R}^{11}$ and R^{12} are the same or different and represent a hydrogen atom, a halogen atom, an alkyl group

having 6 or less carbon atoms or a phenyl group, and each of m and n is an integer of from 0 to 25, provided that at least one of m and n is not 0.

2. (Previously Presented) A process according to claim 1, wherein the mixture in an amount of 20 % to 70 % based on the total amount thereof is charged into a reactor in advance and the balance of 30 to 80 % is added with the advance of the reaction.

3. (Original) A process according to claim 1, wherein the copper-containing catalyst in an amount of 20 to 100 % based on the total amount thereof is charged in a reactor in advance and the balance of 0 to 80 % is added with the advance of the reaction.

4. (Original) A process according to claim 1, wherein the monovalent phenol of the formula (3) is 2,6-dimethylphenol alone or a mixture of 2,6-dimethylphenol and 2,3,6-trimethylphenol.

5. (Original) A process according to claim 1, wherein the molar ratio of the bivalent phenol of the formula (2) and the monovalent phenol of the formula (3) is 1:1 to 1:15.